

Serial No.: 09/485,277

B1
BEROL is between 100 and 200 g/l, particularly favourable is approx. 150 g/l. The most preferable type of BEROL used for this process step is one of the commercially available products from Berol-Kemie Ltd., 44401 Stennungsund, Sweden.--

Please replace the paragraph beginning at page 7, line 7, with the following rewritten paragraph:

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--The deaerated spinning solution is introduced by means of spinnerets into a regenerating bath, preferably at a temperature of between 35 and 45°C, and ideally at a temperature of approx. 40°C. A suitable regenerating bath contains between 70 and 160 g/l of sulphuric acid, preferred is between 90 and 140 g/l, and approx. 120 g/l is ideal, plus between 0.3 and 4 g/l of zinc sulphate, preferred is between 0.5 and 2 g/l, and approx. 1 g/l is ideal, plus between 0.05 and 1 g/l of BEROL, preferred is between 0.1 and 0.7 g/l, and approx. 0.4 g/l is ideal. The most preferable type of BEROL used for this process step is one of the commercially available products from Berol-Kemie Ltd., 44401 Stennungsund, Sweden. The spinnerets used can be oval to long-slit-shaped, and are heated to keep them within a preferred temperature range of 55 - 75°C, particularly favourable is between 65 and 70°C, and approx. 67°C is absolutely ideal.--

IN THE CLAIMS:

1. (Once amended) A process to manufacture a cellulose fibre from hydrate cellulose, the method comprising the following steps:

a) treating wood pulp derived from shoots no older than 1 year of deciduous trees or conifers with an alkali metal hydroxide solution to obtain an alkali cellulose;

b) pressing out superfluous alkali metal hydroxide solution from the alkali cellulose;

c) shredding the alkali cellulose into alkali cellulose crumbs;

d) ripening the alkali cellulose crumbs to a maturity of between 5° and 30°

Hottenroth to form ripened crumbs;

e) treating the ripened crumbs with a wet sulphide process to form sulphadised cellulose;

f) rinsing and diluting of the sulphadised cellulose with water to obtain a spinning solution;

g) ripening of the spinning solution to a maturity of between 5° and 30° Hottenroth;

h) filtering and downstream deaerating the spinning solution;

i) injecting the spinning solution into a regenerating bath under application of spinnerets;

j) stripping the coagulating fibres off of the spinnerets with simultaneous twisting in order to obtain twisted fibres;

k) dehydrating the twisted fibres;

l) desulphurising the twisted fibres;

m) washing the twisted fibres with water;

n) predehydrating the twisted fibres; and

o) drying the twisted fibres.

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3. (Once Amended) Process in accordance with Claim 1, characterised in that the lignin content of the less-than-one-year-old shoots used does not exceed 7%.

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20. (Once Amended) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains between 70 and 160 g/l of sulphuric acid.

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21. (Once Amended) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains between 0.3 and 4 g/l of zinc sulphate.

22. (Once Amended) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains between 0.5 and 1 g/l of BEROL.

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24. (Once Amended) Process in accordance with Claim 23, characterized in that the spinnerets are kept at a temperature of between 65°C and 70°C.

B7
37. (Twice Amended) Fabric comprising:
a) a backing fabric; and
b) a pile comprising fibers in accordance with Claim 33;
wherein the pile is woven into the backing fabric.

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38. (Once Amended) Fabric in accordance with Claim 37, characterized in that the backing fabric has a lattice structure.

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43. (Once Amended) Fabric comprising a backing fabric and a pile woven into the backing fabric comprising cellulose fibers formed by:

- a) treating wood pulp derived from shoots no older than 1 year of deciduous trees or conifers with an alkali metal hydroxide solution in order to obtain an alkali cellulose;
- b) pressing out the superfluous alkali metal hydroxide solution from the obtained alkali cellulose;
- c) shredding the alkali cellulose into crumbs;
- d) ripening the alkali cellulose crumbs to a maturity of between 5° and 30° Hottenroth;
- e) employing a wet sulfide process to treat the ripened crumbs in order to sulfadize the cellulose;
- f) rinsing and diluting the sulfadized cellulose with water in order to obtain a spinning solution;

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- g) subsequently ripening the rinsed and diluted cellulose to a maturity of between 5° and 30° Hottenroth;
 - h) filtering and deaerating the spinning solution
 - i) injecting the spinning solution into a regenerating bath under application of spinnerets;
 - j) stripping off the coagulating fibers with simultaneous twisting in order to obtain twisted fibers;
 - k) dehydrating the twisted fibers;
 - l) desulfurizing the twisted fibers;
 - m) washing the twisted fibers with water;
 - n) predehydrating the twisted fibers; and
 - o) drying the twisted fibers;

the fabric characterised in that the pile consists of 50% oval fibers and 50% tape fibers.

44. (Once Amended) Fabric comprising a backing fabric and a pile woven into the backing fabric comprising cellulose fibers formed by:

- a) treating wood pulp derived from shoots no older than 1 year of deciduous trees or conifers with an alkali metal hydroxide solution in order to obtain an alkali cellulose;
- b) pressing out the superfluous alkali metal hydroxide solution from the obtained alkali cellulose;
- c) shredding the alkali cellulose into crumbs;
- d) ripening the alkali cellulose crumbs to a maturity of between 5° and 30° Hottenroth;
- e) employing a wet sulfide process to treat the ripened crumbs in order to sulfadize the cellulose;
- f) rinsing and diluting the sulfadized cellulose with water in order to obtain a spinning solution;

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- g) subsequently ripening the rinsed and diluted cellulose to a maturity of between 5° and 30° Hottenroth;
 - h) filtering and deaerating the spinning solution
 - i) injecting the spinning solution into a regenerating bath under application of spinnerets;
 - j) stripping off the coagulating fibers with simultaneous twisting in order to obtain twisted fibers;
 - k) dehydrating the twisted fibers;
 - l) desulfurizing the twisted fibers;
 - m) washing the twisted fibers with water;
 - n) predehydrating the twisted fibers; and
 - o) drying the twisted fibers;

the fabric characterized in that the pile consists of 50% of oval fibers with a count of 330 dtex F60 and 50% of tape fibers with a count of 300 dtex F80.

45. (Twice Amended) A cleaning and decontamination fabric made in accordance with Claim 37.

46. (Twice Amended) A water surface tension reducer comprising a fabric in accordance with Claim 37.

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47. (Twice Amended) A textile comprising a fabric in accordance with Claim 37.

48. (Twice Amended) A clothing textile comprising a fabric in accordance with Claim 37.

49. (Twice Amended) A personal hygiene article comprising a fabric in accordance with Claim 37.

50. (Twice Amended) A particle filter comprising a fabric in accordance with Claim 37.

51. (Twice Amended) A condensation catalyst comprising a fabric in accordance with Claim 37.

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52. (Twice Amended) A floor covering comprising a fabric in accordance with Claim 37.

53. (Twice Amended) A covering material comprising a fabric in accordance with Claim 37.

54. (New) Process in accordance with claim 1, characterized in that the lignin content of the less-than-one-year-old shoots used does not exceed 5%.

55. (New) Process in accordance with claim 1, characterized in that the lignin content of the less-than-one-year-old shoots used does not exceed 2%.

56. (New) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains between 90 and 140 g/l of sulphuric acid.

57. (New) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains approximately 120 g/l of sulphuric acid.

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58. (New) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains between 0.5 and 2 g/l of zinc sulphate.

59. (New) Process in accordance with Claim 1, characterized in that the regenerating bath in Step i) contains approximately 1 g/l of zinc sulphate.